



Biotechnology and Industrial Microbiology

Statistical optimization of kojic acid production by a UV-induced mutant strain of *Aspergillus terreus*



Mojtaba Shakibaie^{a,b}, Atefeh Ameri^{c,*}, Roya Ghazanfarian^d, Mahboubeh Adeli-Sardou^a, Sahar Amirpour-Rostami^c, Masoud Torkzadeh-Mahani^e, Mehdi Imani^f, Hamid Forootanfar^{b,c,**}

^a Herbal and Traditional Medicines Research Center, Kerman University of Medical Sciences, Kerman, Iran

^b Department of Pharmaceutical Biotechnology, Faculty of Pharmacy, Kerman University of Medical Sciences, Kerman, Iran

^c Pharmaceutics Research Center, Institute of Neuropharmacology, Kerman University of Medical Sciences, Kerman, Iran

^d The Student Research Committee, Faculty of Pharmacy, Kerman University of Medical Sciences, Kerman, Iran

^e Department of Biotechnology, Research Institute for Science and High Technology and Environmental Sciences, Graduated University of Advanced Technology, Kerman, Iran

^f Department of Basic Sciences, Faculty of Veterinary Medicine, Urmia University, Urmia, Iran

ARTICLE INFO

Article history:

Received 29 September 2017

Accepted 21 March 2018

Available online 24 April 2018

Associate Editor: Gisele Monteiro

Keywords:

Kojic acid

Aspergillus terreus

UV mutagenesis

Medium optimization

ABSTRACT

The ability of four *Aspergillus* strains for biosynthesis of kojic acid was evaluated among which *Aspergillus terreus* represented the highest level (2.21 g/L) of kojic acid production. Improvement kojic acid production ability of *A. terreus* by random mutagenesis using different exposure time to ultraviolet light (5–40 min) was then performed to obtain a suitable mutant of kojic acid production (designated as C₅₋₁₀, 7.63 g/L). Thereafter, design of experiment protocol was employed to find medium components (glucose, yeast extract, KH₂PO₄ (NH₄)₂SO₄, and pH) influences on kojic acid production by the C₅₋₁₀ mutant. A 2⁵⁻¹ fractional factorial design augmented to central composite design showed that glucose, yeast extract, and KH₂PO₄ were the most considerable factors within the tested levels ($p < 0.05$). The optimum medium composition for the kojic acid production by the C₅₋₁₀ mutant was found to be glucose, 98.4 g/L; yeast extract, 1.0 g/L; and KH₂PO₄, 10.3 mM which was theoretically able to produce 120.2 g/L of kojic acid based on the obtained response surface model for medium optimization. Using these medium compositions an experimental maximum Kojic acid production (109.0 ± 10 g/L) was acquired which verified the efficiency of the applied method.

© 2018 Sociedade Brasileira de Microbiologia. Published by Elsevier Editora Ltda. This is an open access article under the CC BY-NC-ND license (<http://creativecommons.org/licenses/by-nc-nd/4.0/>).

* Corresponding author for UV-induced mutagenesis.

** Corresponding author for optimization of kojic acid production.

E-mails: a.ameri@kmu.ac.ir (A. Ameri), h.forootanfar@kmu.ac.ir (H. Forootanfar).

<https://doi.org/10.1016/j.bjm.2018.03.009>

1517-8382/© 2018 Sociedade Brasileira de Microbiologia. Published by Elsevier Editora Ltda. This is an open access article under the CC BY-NC-ND license (<http://creativecommons.org/licenses/by-nc-nd/4.0/>).

Introduction

Kojic acid (KA), 5-hydroxy-2-(hydroxymethyl)-4H-pyran-4-one (Fig. 1), was initially obtained from *Aspergillus oryzae* cultivated on steamed rice (named as “koji” in Japanese) in 1907.^{1,2} This whitening agent could be crystallized as colorless and prismatic needles and chemically classified as a multifunctional, reactive γ -pyrone with weakly acidic properties.^{2,3} KA as a secondary metabolite was usually biosynthesized by several *Aspergillus* and *Penicillium* species as well as some bacterial strains like *Acetobacter* and *Brevibacterium*.^{2,4,5} It has several biotechnological applications and widely used in various area including food, medical, and chemical industries.^{6–8} In addition, KA as a metal chelating agent with tyrosinase inhibition ability has been extensively applied in cosmetic and pharmaceutical industries.^{7,9,10}

Such valuable metabolites production improvement could be attained either by manipulation of the microbial strains or optimization of the fermentation process.^{11,12} Random mutation and selection the best mutant possess extensive application for improvement of the industrially valuable strains.^{13,14} Simple irradiation by ultraviolet (UV) light or gamma ray might induce a mutant with overproduction ability for a selected metabolite which can increase the efficiency and productivity.^{15,16}

Medium optimization and mathematical modeling are among other procedures applied for overproduction of a metabolite in biotechnology.^{16–19} Growth of cells and metabolite concentrations are highly influenced by medium compositions and culture conditions.^{16,20} It is not easy to investigate all the effective factors and their optimum levels by traditional method which evaluates one factor while keep other factors constant.^{20–23} Design of experiments is a group of mathematical and statistical techniques to decrease the total number of experiments, thus aiming for reduction of both costs and time.^{18,20,21}

The present study was aimed to develop an *Aspergillus* mutant strain with high ability of KA production using UV irradiation method. Furthermore, the main factors affecting KA biosynthesis by the selected mutant were screened and the related model was evaluated. On the other hand, this research tried to increase KA production by a simple mutation method combined with medium optimization using statistical experimental design.

Materials and methods

Chemicals and fungal strains

Sucrose, glucose, sodium nitrate (NaNO_3), potassium dihydrogen phosphate (KH_2PO_4), magnesium sulfate heptahydrate ($\text{MgSO}_4 \cdot 7\text{H}_2\text{O}$), potassium chloride (KCl), ferrous sulfate ($\text{FeSO}_4 \cdot 7\text{H}_2\text{O}$), ferric chloride (FeCl_3), yeast extract, Sabouraud dextrose broth (SDB), potato dextrose broth (PDB), and KA were supplied by Merck Chemicals (Darmstadt, Germany). Four *Aspergillus* strains including, *A. flavus* (PTCC 5004), *A. fumigatus* (PTCC 5009), *A. terreus* (PTCC 5283), *A. niger* (PTCC 5012),

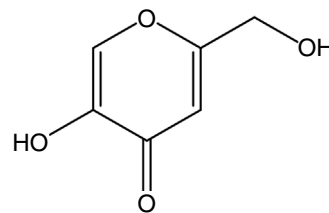


Fig. 1 – The chemical structure of Kojic acid.

and *A. oryzae* (PTCC 5163) were provided by Persian type culture collection (PTCC, Tehran, Iran).

Determination of KA concentration

For determination of KA concentration, Bentley's modified method was used based on the complexation of KA with Fe^{3+} ions and subsequent measurement the absorbance of the produced red complex at 500 nm.²⁴ Briefly, 100 μL from different concentrations of KA (1–32 mg/mL) was transferred to the test tubes containing 900 μL of deionized water and 2 mL of the freshly prepared FeCl_3 (0.06 M) in HCl (0.1 M) was added. After mixing the reagents with 12 mL of deionized water, the absorbance of the mixtures was measured at 500 nm using a UV-Vis spectrophotometer (UV-1800, Shimadzu Corporation, Tokyo, Japan). Deionized water was replaced by KA stocks as blank. All of the above-mentioned procedures were repeated three times on three different days and the mean of absorbencies was used for drawing the suitable standard curve.

Screening of KA producers

Into 50 mL of sterile defined medium consisting glucose (30 g/L); NaNO_3 (2 g/L); KH_2PO_4 (1 g/L); $\text{MgSO}_4 \cdot 7\text{H}_2\text{O}$ (0.5 g/L); KCl (0.5 g/L); and $\text{FeSO}_4 \cdot 7\text{H}_2\text{O}$ (0.01 g/L) 1 mL of spore stock suspension (1×10^8 spore per mL) of *A. flavus*, *A. fumigatus*, *A. terreus*, *A. niger*, and *A. oryzae* was separately added and each 250-mL inoculated Erlenmeyer flask was then incubated in a shaker incubator (30 °C, 150 rpm) for a period of 30 days. Interval samples (1 mL) were consequently withdrawn aseptically each 24 h. Fungal cells were then harvested by centrifugation (6000 $\times g$, 20 min) and the obtained supernatants were used to determine the KA concentrations in the media in comparison with that of the blank (the supernatant obtained from the un-inoculated media) as previously described (see “Determination of KA concentration” section). These experiments were reiterated three times on various days.

UV-induced mutagenesis

The highest KA producer strain was cultivated on potato dextrose agar (PDA) plates for seven days at 30 °C. Then, the produced spores were collected and washed in triplicate with sterile normal saline by sequential centrifugation (7000 $\times g$, 10 min). Different test tubes containing the spore suspensions in sterile normal saline solution (OD_{600} , 0.1, 4 mL) were then exposed to UV light in a cabinet containing UV lamp (255 nm) placed at 20 cm distance from the test tube surface. After 5 min, 10 min, 20 min, and 40 min each UV exposed spore

Table 1 – Applied levels of independent variables in the fractional factorial design.

Variable	Component	Unit	Low level (–1)	High level (+1)
X ₁	Glucose	g/L	50	100
X ₂	Yeast extract	g/L	0.5	1
X ₃	KH ₂ PO ₄	mM	0.5	14
X ₄	pH	–	2	5
X ₅	(NH ₄) ₂ SO ₄	g/L	0.5	2

suspension was stored in the dark overnight followed by serially diluting each spore suspension in phosphate buffer solution (pH 7) and spreading of each sample on PDA plate. The numbers of viable colonies on each plate were then counted after 7 days incubation at 30 °C. For isolation of mutants with KA biosynthesis ability, the plates exhibited less than 1% survival rate were selected.¹⁴

Screening of high KA producer mutants and determination of culture conditions

Screening of mutants with the ability for production of KA was done in 96-well microplates. Firstly, 100 µL of UV induced mutant spores (OD₆₀₀, 0.1) survived from the previous section were separately transferred to wells containing PDB (100 µL). After 24 h, 48 h, and 72 h incubation at 30 °C, 10 µL of ferric chloride solution (1%) were separately added to each well and the absorbance was then measured at 500 nm with a Synergy 2 multimode microplate reader (Biotek, USA). The mean of absorbance from three independent tests was used for comparing with the results from cells which did not expose to UV light and selecting the high KA producer mutant.¹⁴ The selected mutant was then preserved at –80 °C in glycerol (20%) supplemented SDB medium. Thereafter, one mL spore suspension (1 × 10⁸ spores per mL) obtained from the wild-type cells and the selected mutant was separately cultivated in 250-mL Erlenmeyer flasks containing the defined medium (50 mL) with and without shaking (30 °C, 30 days) and KA concentration was periodically measured.

Experimental design

A two-step experimental design was used for screening the most effective factors in KA production by the selected *Aspergillus* mutant and for developing a mathematical model for optimal conditions. The factors including, glucose concentration (X₁), yeast extract concentration (X₂), KH₂PO₄ amount (X₃), initial pH of culture media (X₄), and (NH₄)₂SO₄ concentration (X₅) were selected. Table 1 exhibited the range of the selected factors. Fractional factorial design (FFD) was then applied to screen the most efficient factors affecting KA production. Statistical software, Design-Expert version 7.0.0 (Stat-Ease, Inc., Minneapolis, MN, USA), was employed for designing a 2^{5–1} FFD with 5 center points (Table 2, Run 1–21). Coding of the variables was done according to the following equation:

$$x_i = \frac{X_i - X_{i;0}}{\Delta X} \quad i = 1, 2, 3, \dots, k \quad (1)$$

Table 2 – Experimental design and results of the 2^{5–1} FFD augmented to central composite design.

Run	Coded levels					KA concentration (g/L)	
	x ₁	x ₂	x ₃	x ₄	x ₅	Experimental	Predicted
1	–1	–1	–1	–1	+1	12.1	13.7
2	+1	–1	–1	–1	–1	12.3	16.0
3	–1	+1	–1	–1	–1	25.2	40.5
4	+1	+1	–1	–1	+1	36	51
5	–1	–1	+1	–1	–1	1.0	1.5
6	+1	–1	+1	–1	+1	10.5	2.4
7	–1	+1	+1	–1	+1	1.5	2.3
8	+1	+1	+1	–1	–1	98.2	122.5
9	+1	–1	–1	+1	–1	19.9	39.4
10	+1	–1	–1	+1	+1	12.2	19.4
11	–1	+1	–1	+1	+1	14.9	17.8
12	+1	+1	–1	+1	–1	22.2	33.5
13	–1	–1	+1	+1	+1	5	6.2
14	+1	–1	+1	+1	–1	15.6	17.1
15	–1	+1	+1	+1	–1	3.7	5.3
16	+1	+1	+1	+1	+1	9.5	15.6
17	0	0	0	0	0	15.1	24.7
18	0	0	0	0	0	16.4	24.7
19	0	0	0	0	0	28.9	24.7
20	0	0	0	0	0	10.75	24.7
21	0	0	0	0	0	28.6	24.7
22	–2	0	0	0	0	10	8.1
23	2	0	0	0	0	97	76
24	0	–2	0	0	0	14.4	8.6
25	0	+2	0	0	0	118.2	70.9
26	0	0	–2	0	0	5.2	3.5
27	0	0	2	0	0	20.3	13.8
28	0	0	0	–2	0	24.5	14.7
29	0	0	0	+2	0	19.2	14.7
30	0	0	0	0	–2	27.1	24.7
31	0	0	0	0	+2	33.5	24.7
32	0	0	0	0	0	27.4	24.7
33	0	0	0	0	0	47.5	24.7

where x_i is the coded value of an independent variable, X_i is the independent variable's real value, X_{i;0} is the independent variable's real value at the center point, and ΔX_i is the step change value. Dependent variable (or response) was defined as KA concentration. The runs were randomly carried out trying to nullify the effect of nuisance variables. After analyzing the results and finding a significant curvature, the 2^{5–1} FFD was augmented to a central composite design (CCD) by adding 12 new experiments (Table 2, Run 22–33) to the previous design. The chosen variables can be related to the response by the model as shown in the following equation:

$$Y = b_0 + \sum_{i=1}^n b_i x_i + \sum_{i=1}^n b_{ii} x_i^2 + \sum_{i=1}^{n-1} \sum_{j=i+1}^n b_{ij} x_i x_j + e \quad (2)$$

In this equation x_i (i = 1–5) are the variables of the experiment, Y is response function (KA production), e is the error of the experiment, b₀ is the constant coefficient, b_i (i = 1–5) are the linear coefficients, b_{ij} (i ≠ j) are the second-order coefficients, b_{ii} (i = 1–4) are the second-order interaction coefficients, and x are the independent variables, where in this study independent variables were coded as A, B, C, D, and E.

Finally, the predicted model was affirmed for variables applied in the design.

Data analysis

Design-Expert version 7.0.0 statistical software was used for analysis of the results. The coefficient of determination, R^2 was applied for evaluating the qualities of the fitted model. In addition, analysis of variance (ANOVA) together with the F-test was used for assessing the effects and $p \leq 0.05$ was considered as significant. The location of the optimum was estimated by solving the fitted model.

Results

Screening of a high level KA producer strain and mutant

Among four tested fungal strains, *A. terreus* showed the highest level of KA production (2.21 g/L, Fig. 2A). The amount of KA

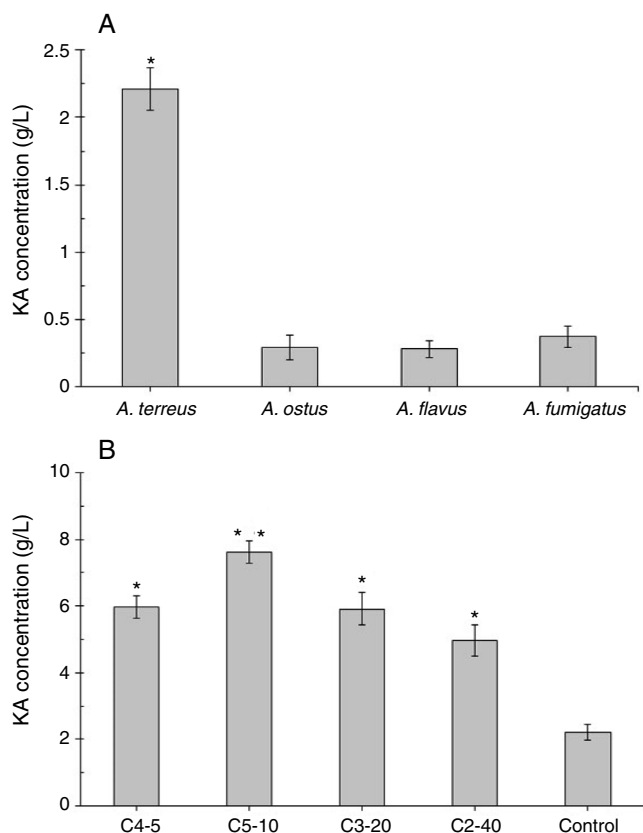


Fig. 2 – (A) Screening of a high level KA producing *Aspergillus* strain. Significant values (*) were determined after ANOVA analysis with Dunnett's T3 post hoc test (p -value < 0.05). (B) Screening the best mutants of *A. terreus* after different exposure time to UV light irradiation compared with the wild strain of *A. terreus* (as a positive control). Significance (*) was evaluated after ANOVA analysis of the obtained results (p -value < 0.05). Significance of the C5-10 mutant results (□) was also checked in comparison with other groups (C4-5, C3-20, and C2-40, p -value < 0.05).

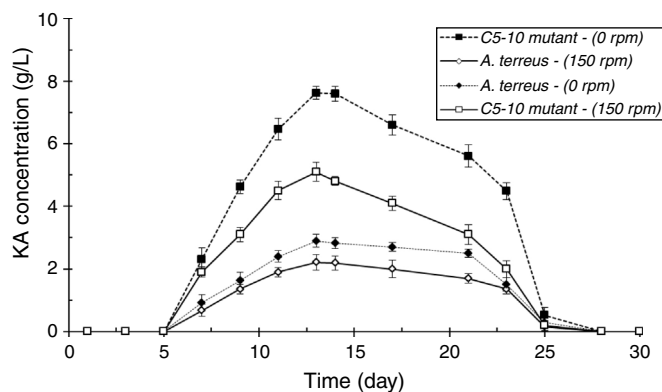


Fig. 3 – Time course study of KA production by wild strain of *A. terreus* and C5-10 mutant in different culture conditions.

produced by *A. fumigatus* (0.37 g/L), *A. ostus* (0.29 g/L), and *A. flavus* (0.28 g/L) was not significantly different from each other ($p > 0.05$). Irradiated samples were grown on PDA for 4 days and sub-cultured in 96-well microplates. The obtained results showed that few variants exhibited more intense deep red color than the wild strain after adding ferric chloride solution (1%). The C4-5, C5-10, C3-20, and C2-40 mutants exposed to UV light for 5 min, 10 min, 20 min, and 40 min, respectively were selected as high KA producers (Fig. 2B). Fig. 3 exhibited the time course of KA production by *A. terreus* and C5-10 mutant cultured in defined media with and without shaking at 30 °C. For wild and selected mutant strain the maximum KA production was observed 13 days after the spore inoculation in static incubation condition (2.9 g/L and 7.62 g/L, respectively).

Experimental design

Five medium ingredients were assessed at selected levels (Table 1). The KA concentration results for an augmented 2^{5-1} FFD with the levels in coded units are represented in Table 2. The response range was from 1.0 g/L to 118.2 g/L thus, a logarithmic transformation was required. To summarize the analysis of the response effects and evaluate the significance of the model terms, the ANOVA table was created (Table 3). A second-order polynomial expression was fitted on CCD results. The fitted model (in the terms of coded values) for estimating KA production by the selected mutant was:

$$\begin{aligned} \log_{10}(\text{KA concentration}) = & 1.39 + 0.24x_1 + 0.23x_2 + 0.15x_3 \\ & + 0.077x_1x_2 + 0.23x_1x_3 - 0.13x_1x_4 \\ & - 0.14x_2x_4 - 0.11x_2x_5 - 0.14x_3^2 \\ & - 0.056x_4^2 - 0.12x_1^2x_2 - 0.36x_1^2x_3 \\ & - 0.069x_1^2x_5 \end{aligned} \quad (3)$$

To support the hierarchy of the model, X_4 and X_5 were not eliminated. The calculated F-value (24.9) for the selected model implied that it was significant (Table 3). The related residual vs. predicted response obtained from the final model

Table 3 – Analysis of variance for CCD refined model.

Source of variation	Sum of square	df	Mean of square	F value	Prob > F
Model	5.35	13	0.41	24.98	<0.0001
x_1	1.43	1	1.43	86.56	<0.0001
x_2	0.42	1	0.42	25.35	<0.0001
x_3	0.17	1	0.17	10.61	0.0044
x_1x_2	0.095	1	0.095	5.74	0.0277
x_1x_3	0.82	1	0.82	50.03	<0.0001
x_1x_4	0.29	1	0.29	17.44	0.0006
x_2x_4	0.29	1	0.29	17.73	0.0005
x_2x_5	0.19	1	0.19	11.51	0.0032
x_3^2	0.57	1	0.57	34.77	<0.0001
x_4^2	0.096	1	0.096	5.82	0.0267
$x_1^2x_2$	0.078	1	0.078	4.71	0.0436
$x_1^2x_3$	0.70	1	0.70	42.44	<0.0001
$x_1^2x_5$	0.076	1	0.076	4.59	0.0461
Residual	0.3	18	0.016		
Lack of fit	0.13	13	0.0099	0.29	0.9655
Pure error	0.17	5	0.034		
Cor total ^a	6.44	32			

^a $p < 0.001$

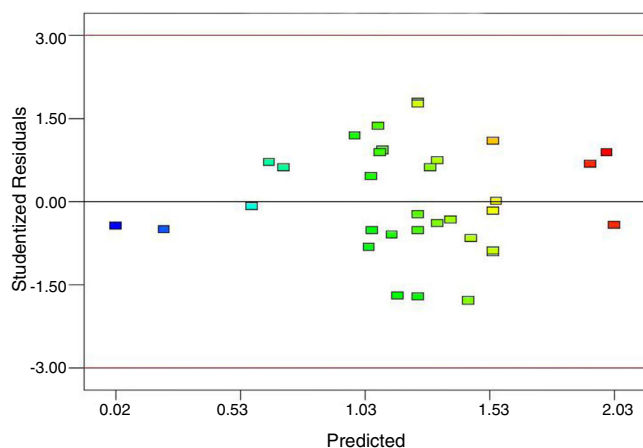


Fig. 4 – Studentized residuals against predicted response by final quadratic model.

is illustrated in Fig. 3 from which a nearly constant variance throughout the response range was obvious. The 3-D counter plots were shown in Fig. 4 supported by the selected model.

Discussion

Screening of different species of *Aspergillus* genera to obtain a high level KA producer was previously reported by El-Kady et al.⁸ among which *A. flavus*, *A. phoenicis*, and *A. wentii* were found to produce 5 g/L of KA in submerged fermentation. In another study, Hazzaa et al.² described about the KA biosynthesis ability of *Aspergillus* strains including, *A. oryzae* var. *effusus* NRC14 (42.0 g/L), *A. flavus* NRC13 (41.0 g/L), *A. tamarii* NRC18 (22.0 g/L), and *A. parasiticus* (17.7 g/L). Improvement the KA production ability of *A. terreus* by random mutagenesis using UV light irradiation (for 5, 10, 20, and 40 min) was also performed in this study to get a potent mutant which produce

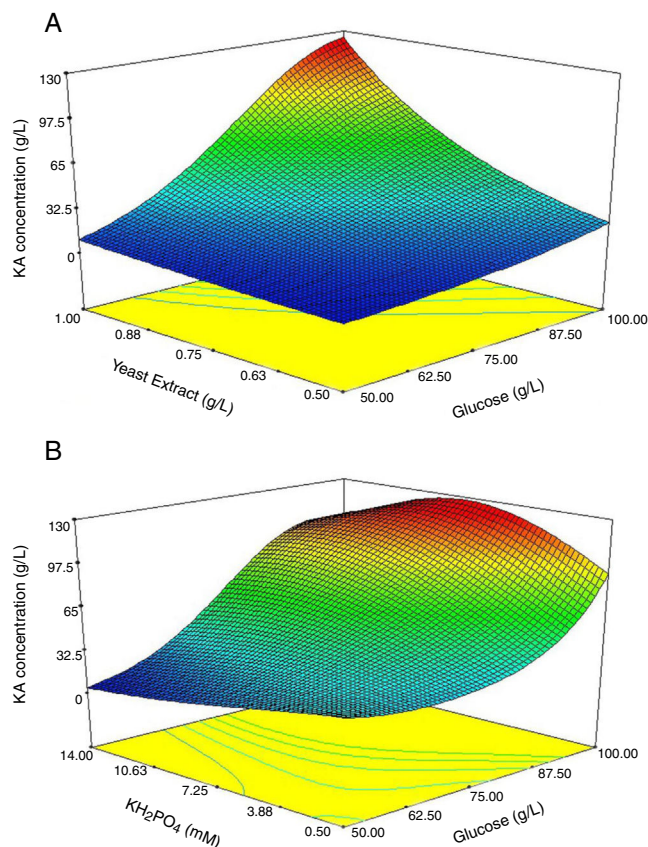


Fig. 5 – Response surface graphs of produced KA concentration (A) and (B) constant level of KH_2PO_4 and yeast extract concentrations at their optimum points, respectively.

KA higher than its wild strain. The amount of KA produced by C_{4-5} , C_{3-20} , and C_{2-40} mutants was significantly higher than their wild *A. terreus* ($p < 0.05$) after 13 days incubation (30 °C, 150 rpm). Furthermore, it was found that C_{5-10} was the most potent KA producer mutant (7.62 g/L, $p < 0.05$). Similar results were reported by Mohamad et al.³ who observed a 100-fold increase of KA productivity of *A. oryzae* ATCC 22788 after UV-induced mutagenesis. El-Aziz⁴ found that the KA yield of the most efficient UV-induced mutant was 120% higher than the wild strain of *A. flavus*. Incubation with shaking significantly reduced the KA production yields by *A. terreus* and C_{5-10} mutant ($p < 0.05$, Fig. 5). These results were in contrast with the results reported by El-Aasar¹ who observed that both mycelial growth rate and KA production of *A. parasiticus* decreased in the static fermentation states compared with those of shaking cultures.

In the first step of the optimization procedure, identification of the medium component(s) harboring significant effect on KA production by C_{5-10} mutant was aimed. For glucose (X_2) the measured p -value was less than 0.05 (Table 3), so this parameter had a significant effect on KA production by C_{5-10} mutant. Hassan et al.²⁵ showed that glucose was the best carbon source for KA production followed by sucrose, fructose, and starch, which enhanced the KA amount to 49.0, 38.0, 34.0, and 26.0 g/L, respectively. Glucose, as a monosaccharide, was

used as a carbon source for biomass built-up and it was also used as a suitable precursor for KA biosynthesis by *Aspergillus* strains.^{3,25} Kitada et al.²⁶ reported that all supplied glucose at the concentration of 25 g/L and 50 g/L was consumed for biomass built-up by *A. oryzae*. However, the highest KA production by *A. oryzae* (24.2 g/L) was obtained in the presence of 100 g/L of glucose in the culture media.²⁶

Analysis of variance of the obtained results in the case of yeast extract (X_2) showed that this factor was also significantly affected the KA production by C_{5-10} mutant ($p < 0.05$) (Table 3). Organic nitrogen sources are generally better than inorganic nitrogen supplements for KA fermentation due to the presence of buffering system, vitamins, and oligoelements.^{7,27} Beside the peptone and polypeptone, yeast extract has been reported to be a favorable organic nitrogen source for KA production.^{1,16} However, Kwak and Rhee²⁸ reported a high production yield for KA (83 g/L) by *A. oryzae* using a mixture of yeast extract and $(\text{NH}_4)_2\text{SO}_4$ as nitrogen sources.

For KH_2PO_4 (X_3) the measured p -value was less than 0.05 (Table 3), so, this factor was also considerably affected the KA production by C_{5-10} mutant. Rapid KA production was previously observed in the culture broth containing phosphate ranging from 0.55 mM to 13.72 mM.^{3,29} On the other hand, Coupland and Niehaus³⁰ reported that production of KA by *A. flavus* was not influenced by phosphate concentrations in the range of 0.1 mM to 100 mM.

Previous studies confirmed that the optimal pH for biosynthesis of KA by different strain of *A. oryzae* was ranged from 3 to 6.^{16,25} Rosfarizan et al.³¹ considered that the highest KA production achieved at the pH range of 2–3. In another study, it was found that the maximum KA was biosynthesized by *A. oryzae* var. *effusus* NRC14 and *A. flavus* NRC13 in a culture medium with initial pH equal to 4.² Katagiri and Kitahara³² reported that the optimal pH of cultural media (pH 5) for *A. oryzae* growth was significantly higher than optimal pH for KA production (pH 2.4). However, in the present study the KA production of the mutant strain C_{5-10} was not significantly affected by pH (X_4) and $(\text{NH}_4)_2\text{SO}_4$ amount (X_5) within the tested levels (Table 3).

For fitted model (Eq. (3)), the measured p -value indicated the significant model with a probability level of 95%. In addition, the significant F -value of the model revealed that there was only 0.01% chance that the “Model F -value” was take place by noise. The relatively high value of $R^2 = 0.9475$ implied that the model was a significant fitness. Also, “lack of fit F -value” was measured as 0.29 which was not different from the pure error. There is a 97.5% chance that this F -value for lack of fit could occur due to the noise. The predicted R^2 (0.7967) was reasonably confirmed by adjusted R^2 (0.9095). A desirable signal to noise ratio was confirmed by measured adequate precision (23.2), thus the selected model can be used in the design space. Adequate precision values mentioned above supported the hypothesis that the model equation was sufficient to describe the response of the experimental observations relating to the KA production. The predicted KA concentrations by the selected model are given in Table 2 which exhibited a good agreement between the predicted and experimental data. Furthermore, the optimal level of three effective factors was determined to be 98.4 g/L of glucose, 1.0 g/L of yeast extract, and 10.3 mM of KH_2PO_4 obtained by alteration the

factor levels of the selected model. By replacing these levels in the selected model an optimal amount of 120.2 g/L KA was predicted. The suggested optimum medium composition was repeatedly (three times) used for testing the model adequacy. The KA concentration in these three independent experimental tests was 109.0 ± 10 g/L which exhibited a suitable agreement with the predicted results.

Fig. 4A exhibited the response surface curve for the constant level of KH_2PO_4 (10.3 mM) while glucose and yeast extract were changed within their experimental levels. The minimum response (1.5 g/L) occurred when both glucose (50 g/L) and yeast extract (0.50 g/L) were at their lowest level. The obtained results showed that in the presence of high level of yeast extract (1 g/L) and glucose (100 g/L) the maximum level of KA production occurred (Fig. 4A). Furthermore, when glucose was at low or high levels, KA production by C_{5-10} mutant was not considerably changed at a low level of yeast extract (0.5 g/L) (Fig. 4A). Analysis of the response at the different levels of the factors revealed that there is a remarkable interaction between glucose and yeast extract at the optimum level of KH_2PO_4 . At the optimum level of yeast extract (1 g/L), minimum response (2.45 g/L) was observed with a low level of glucose (50 g/L) and high level of KH_2PO_4 (14 mM) (Fig. 4B). When KH_2PO_4 was at low or high levels, the production of KA by C_{5-10} mutant was not significantly different at the high level of glucose ($p < 0.05$) (Fig. 4B). Furthermore, biosynthesis of KA by C_{5-10} mutant in the presence of 0.5 mM KH_2PO_4 was significantly higher than 14 mM at a low level of glucose (Fig. 4B). Also, the attained results suggested a considerable interaction between glucose and KH_2PO_4 at the optimum level of yeast extract.

Conclusion

The present research was aimed to produce a mutant strain of *A. terreus* with high ability for KA biosynthesis using a conventional UV-induced mutagenesis method followed by application of fractional factorial design to optimize culture media components required for KA production. pH and $(\text{NH}_4)_2\text{SO}_4$ were established not to be very important factors considering to KA production assisted by the mutant strain of C_{5-10} , while glucose, yeast extract, and KH_2PO_4 were represented the significant effect on such ability. Finally, the optimum medium composition for biosynthesis of KA by C_{5-10} mutant was determined as follows; glucose (98.4 g/L), yeast extract (1.0 g/L), KH_2PO_4 (10.3 mM), initial pH of culture media equal to 2.1, and $(\text{NH}_4)_2\text{SO}_4$ (0.82 g/L). More than 50-fold overproduction of KA by C_{5-10} mutant strain of *A. terreus* was achieved using simple mutagenesis and medium optimization methods. However, further studies must be performed to merit potential application of this strain for large-scale production of KA.

Conflicts of interest

The authors declare no conflicts of interest.

Acknowledgements

This work was financially supported by a grant from Herbal and Traditional Medicines Research Center, Kerman University of Medical Sciences (Kerman, Iran) (95000197). Research reported in this publication was also supported by Elite Researcher Grant Committee under award number [965378] from the National Institutes for Medical Research Development (NIMAD), Tehran, Iran.

REFERENCES

1. El-Aasar S. Cultural conditions studies on kojic acid production by *Aspergillus parasiticus*. *Int J Agric Biol*. 2006;8:468–473.
2. Hazzaa M, Saad A, Hassan H, Ibrahim E. High production of kojic acid crystals by isolated *Aspergillus oryzae* var. *effusus* NRC14. *J Appl Sci Res*. 2013;9:1714–1723.
3. Mohamad R, Mohamed MS, Suhaili N, Salleh MM, Ariff AB. Kojic acid: applications and development of fermentation process for production. *Biotechnol Mol Biol Rev*. 2010;5:24–37.
4. Rodrigues APD, Carvalho ASC, Santos AS, Alves CN, Nascimento JLM, Silva EO. Kojic acid, a secondary metabolite from *Aspergillus* sp., acts as an inducer of macrophage activation. *Cell Biol Int*. 2011;35:335–343.
5. Liu JM, Yu TC, Lin SP, Hsu RJ, Hsu KD, Cheng KC. Evaluation of kojic acid production in a repeated-batch PCS biofilm reactor. *J Biotechnol*. 2016;218:41–48.
6. Chaves FC, Gianfagna TJ, Aneja M, Posada F, Peterson SW, Vega FE. *Aspergillus oryzae* NRRL 35191 from coffee, a non-toxicogenic endophyte with the ability to synthesize kojic acid. *Mycol Prog*. 2012;11:263–267.
7. Terabayashi Y, Sano M, Yamane N, et al. Identification and characterization of genes responsible for biosynthesis of kojic acid, an industrially important compound from *Aspergillus oryzae*. *Fungal Gen Biol*. 2010;47:953–961.
8. El-Kady IA, Zohri ANA, Hamed SR. Kojic acid production from agro-industrial by-products using fungi. *Biotechnol Res Int*. 2014;2014:1–10.
9. Synytsya A, Blafková P, Synytsya A, Čopíková J, Spěváček J, Uher M. Conjugation of kojic acid with chitosan. *Carbohydr Polym*. 2008;72:21–31.
10. Coelho R, Anschau A, Monte-Alegre R. Kojic acid production from glycerol: optimization using central composite rotatable design. *J Biotechnol*. 2010;150:84.
11. Ellaiah P, Prabhakar T, Ramakrishna B, Thaer Taleb A, Adinarayana K. Strain improvement of *Aspergillus niger* for the production of lipase. *Indian J Microbiol*. 2002;42:151–153.
12. Watanabe-Akanuma M, Inaba Y, Ohta T. Mutagenicity of UV-irradiated maltol in *Salmonella typhimurium*. *Mutagenesis*. 2006;22:43–47.
13. Adeoye A, Lateef A, Gueguim-Kana E. Optimization of citric acid production using a mutant strain of *Aspergillus niger* on cassava peel substrate. *Biocatal Agric Biotechnol*. 2015;4:568–574.
14. El-Aziz ABA. Improvement of kojic acid production by a mutant strain of *Aspergillus flavus*. *J Nat Sci Res*. 2013;3:31–41.
15. Hsieh HJ, Giridhar R, Wu WT. Regioselective formation of kojic acid-7-o-alpha-d-glucopyranoside by whole cells of mutated *Xanthomonas campestris*. *Enzyme Microb Technol*. 2007;40:324–328.
16. Chaudhary J, Pathak A, Lakhawat S. Production technology and applications of kojic acid. *Ann Rev Res Biol*. 2014;4:3165–3196.
17. Devi KBD, Vijayalakshmi P, Kumar BV. Response surface methodology for the optimization of kojic acid production by *Aspergillus flavus* using Palmyra sap as a carbon source. *Eur J Biotechnol Biosci*. 2014;2:52–57.
18. Devi KBD, Vijayalakshmi P, Kumar BV, Talluri VP. Statistical optimization of kojic acid production through response surface methodology by *Aspergillus flavus* using sago starch hydrolysate as a carbon source. *Asian J Appl Sci Eng*. 2014;3:421–428.
19. Aghaie-Khouzani M, Forootanfar H, Moshfegh M, Khoshayand MR, Faramarzi MA. Decolorization of some synthetic dyes using optimized culture broth of laccase producing ascomycete *Paraconiothyrium variabile*. *Biochem Eng J*. 2012;60:9–15.
20. Devi KBD, Vijayalakshmi P, Shilpa V, Kumar BV. Response surface methodology for the optimization of kojic acid production by *Aspergillus flavus* using Muntingia calabura fruits as a carbon source. *Indian J Sci Technol*. 2015;8:556–561.
21. Hatami M, Cuijpers M, Boot M. Experimental optimization of the vanes geometry for a variable geometry turbocharger (VGT) using a design of experiment (DoE) approach. *Energy Convers Manage*. 2015;106:1057–1070.
22. Etezed S, Akbari N, Khajeh K, Dabirmanesh B. Application of half-fractional factorial design (H-FFD) and response surface methodology to optimize conditions for lipase production of a newly isolated *Pseudomonas* sp. *Int J Eng Adv Technol*. 2015;5:8–18.
23. Hasan-Beikdashti M, Forootanfar H, Safarian MS, et al. Optimization of culture conditions for production of lipase by a newly isolated bacterium *Stenotrophomonas maltophilia*. *J Taiwan Inst Chem Eng*. 2012;43:670–677.
24. Bentley R. Preparation and analysis of Kojic acid. *Methods Enzymol*. 1957;3:238–241.
25. Hassan H, Saad A, Hazzaa M, Ibrahim E. Optimization study for the production of kojic acid crystals by *Aspergillus oryzae* var. *effusus* nrc 14 isolate. *Int J Curr Microbiol Appl Sci*. 2014;3:133–142.
26. Kitada M, Ueyama H, Suzuki E, Fukimbara T. Studies on kojic acid fermentation: (I) cultural conditions in submerged culture. *J Ferment Technol*. 1967;45:1101–1107.
27. Gad A. Modification of molasses for kojic acid production by *Aspergillus parasiticus*. *New Egypt J Microbiol*. 2003;5:14–26.
28. Kwak MY, Rhee JS. Controlled mycelial growth for kojic acid production using Ca-alginate-immobilized fungal cells. *Appl Microbiol Biotechnol*. 1992;36:578–583.
29. Arnstein H, Bentley R. The biosynthesis of kojic acid. 1. Production from [1-14C] and [3: 4-14C2] glucose and [2-14C]-1:3-dihydroxyacetone. *Biochem J*. 1953;54:493–508.
30. Coupland K, Niehaus WG. Effect of nitrogen supply, Zn²⁺, and salt concentration on kojic acid and versicolorin biosynthesis by *Aspergillus parasiticus*. *Exper Mycol*. 1987;11:206–213.
31. Rosfarizan M, Arbakariya A, Hassan MA, Karim MIA, Hiroshi S, Suteaki S. Importance of carbon source feeding and pH control strategies for maximum kojic acid production from sago starch by *Aspergillus flavus*. *J Biosci Bioeng*. 2002;94:99–105.
32. Katagiri H, Kitahara K. The formation of kojic acid by *Aspergillus oryzae*: Part I. The formation of kojic acid from pentoses, sugar alcohols and gluconic acid. *J Agric Chem Soc Jpn*. 1929;5:38–47.